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# Design of a lead blast furnace

Walter Irving Phillips

Andrew Jackson Seltzer

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## FOR THE

# Degree of Bachelor of Science

IN

# Chemistry and Metallurgy.

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# SUBJECT:

"Design of a Lead Blast Furnace."

WALTER I. PHILLIPS. A. J. SELTZER. JUNE, 1907.

#### DESIGN OF A 100 TON LEAD BLAST FURNACE.

Calculations for the charge. Calculations for the inside dimensions of Furnace. Calculation of the Furnace gases. Calculation of the size of the tuyers. Drawings of the Furnace.

In order to get the approximate size of the Furnace we made the following assumptions, being guided as far as possible by the practice of the Globe Smelting Works at Denver, Colorado whenever that could be ascertained.

The coke used is that made at Tuscarawas,Ohio,and has the following composition: water 0.13%,volatile matter 2.75%,fixed carbon 84.2%, ash 12.4%,sulphur 3.7%. It was assumed that the S. was **distributed**thus: in volatile matter 1.8%,in ash 1.8% as FeScand Cas04.

The ash analysed as follows:  $SiO_2$  40.3%,  $Fe_2O_3$  29.4%, CaO 6.9, MgO 1.4%,  $Al_2O_3$  20.1%,  $FeS_2$  and  $GaSO_4$  1.8%

The lead ore delivered to the furnace comes from Leadville and has been previously roasted flown to 6.8% and its composition is

SiO<sub>2</sub> FeS Fe<sub>2</sub>O<sub>3</sub> MnO CaO MgO ZnS Al<sub>2</sub>O<sub>3</sub> As PbS Cu<sub>2</sub>S 36.4 6.6 19.3 4.3 4.4 5.26 2.4 2.5 5 14.0 1.83 Ag Au

50.5oz. Trace.

The iron ore is a dry oxidized silver ore from fighdville, Colo., of the following composition:

	Si02	Fe203	MnO	CaCO3	Ag	Au.
	5.3	79.28	1.7	5.5	8.20ź.	.IIoz.
	The limestone	e is of do	lomitic	character	and barre	n of values,obtain-
өđ	from a quarry	y near Den	ver and	is of the	following	composition:

$Si0_2$	FeC03	CaCO <sub>3</sub>	M <b>gC</b> 03
3:7	7.2	75.5	10.3

In order that these metals shall enter the slag they must become exides, and iron will enter the slag only as FeO hence the other exides of iron will have to be calculated over to that exide when figuring up the charge for the furnace. These calculations are made by means of simple ratios of atomic weights and will not be gone into in detail further than to give one example; thus, to determine the  $\frac{19}{3}$  amount of FeO in -19.3#Fe2O3of the lead ore we have:

 $Fe_{2}O_{3}$  : 2FeO = 160: 144 = 19.3# : X X = 17.4# FeO in 100 lbs of ore.

The 6.6 lbs FeS burned to FeO = 5.4 lbs. FeO. Total FeO = 17.4 + 5.4 = 22.8 lbs FeO.

In this manner the following table of adjusted oxides was obtained:

	$sio_2$	FeO	CaO	Zn0		, S	As	$P\mathbf{b}$	Cu.
Lead Ore	36.4	22.8	11.8	2.0	2.5	6.8	.5	12	1.5
Iron "	5.3	73.1	3.1					، م به ر ره	
Limestone	3.7	4.5	49.2						e Santa de la Santa de
Coke Ash	40.3	26.5	8.9		20.1				رکینید میں دی میں فر

Since MnO acts much like FeO in the slag, it is counted as FeO in the adjusted table. Its atomic weight is so near that of FeO that no appreciable error was introduced by adding the weight of the two oxides directly without figuring them over from their atomic weights. MgO acts like CaO in many respects hence it is counted as lime in the table. The weights were figured however from the atomic weights thus: multiply the weight of MgO in the one by 1.4 to get the equivalent weight of GaO for combining with SiOp.

The slag to be calculated is to be 30- 40- 15, which will be liquid, fairly easily fusible at a low temperature and at the same time decrease the amount of barren limestone put into the charge. IRON ORE CALCULATIONS. When buying iron ore for fluxing purposes only the "available" iron is paid for, i.e. the SiO<sub>2</sub> in the flux is not wanted hence the FeO, needed to slag this silica, is deducted before paying for the flux.

1 In 100 lbs. of ore we have 66 lbs FeO available. This result was obtained as follows: - slag is to be 30 - 40 - 15 , hence

30 : 40 = 5.8 : X, or X = 7.4# Fe0 to sleg 5.5# Si0.

73.1 - 7.1 = 66.0# FeO available. This 66.0 lbs Feo. carries 61.1 lb Fe.

No determine how much lime should be added we used the following proportion:

30 : 15 = 5.3 : X, X h 2.6 lbs. CaO. The iron ore carries 3.1 lbs CaO hence it is self fluxing as regards lime.

11 IRON FOR SPEISS. As. is very undesirable in the lead bullion, and if it is present in the ore it must be provided for. Iron forms several alloys with As but the only one which is liquid when fused is Fe<sub>5</sub>As. This is termed "Speiss" and goes with the matte, in the furnace, thus preventing the As from going into the Lead. In 100 lbs. of lead cre we have .5 lbs As. The iron needed for speiss is artained thus:

(5x, 56) : 75 =X : .5, X = 1.9 lbs Fe.

100 lbs iron ore 51.1 = X : 1.9, X = 3.71 lbs. 6% iron ore necessary to form the speiss for 100% lead ore. IRON FOR MATTE. The datte fall should be kept low as considerable lead will otherwise go into it. The matte fall was calculated at 10% and its composition was assumed as follows:

Pb	20%
Ag	• 06%
Au	Trace
Zn	"
SiO2	4,2% (Carried mechanically)
SiO <sub>2</sub> Cu	4,2% (Carried mechanically) 15.0
SiO <sub>2</sub> Cu Fe	4,2% (Carried mechanically) 15.0 37.0

**En** 10 lbs matte have

.38 Lbs. S from 1.88 lbs Cu<sub>3</sub>S .30 " " " 2.30 " PbS \_\_\_\_\_\_ " " <u>5.82</u> " FeS. - 2.80 " " " 10.00 " matte.

5.82 lbs FeS contains 3.7 lbs Fe which is equivalent to 7.2 lbs iron ore.

IV. COKE-ASH CALEULATIONS. Usel2. Africal. Charge to be 1500 lbs 12. XX 1500 =210 lbs coke containing 26.1 lbs. ash composed of the following SiO<sub>2</sub> FeO CaO

10.5# 6.9 2.3 30 : 40 = 10.5 : X, X=  $\frac{1}{4}$  40 1bs Fe0

FeO present in ash 6.9

heeded 7.1 lbs = 10.8 lbs. iron ore. 30: 15 = 10.1 : X = 5.05 lbs CaO needed for 10.5 lbs SiO<sub>2</sub> CaO present in the ash = 2.3#, CaO needed = 5.05 = 8.3 = 2.75 lbs CaO or 5.5 lbs limestone.

4

V. LEAD ORE.

4.2 lbs  $SiO_2$  go to the matte, 100 lbs ore carries 36.4 lbs. SiO<sub>2</sub>, SiO<sub>2</sub> to be fluxed = 36.4 - 4.2 = 32.2 lbs.

30: 40 = 32.2: X, X = 42.9 lbs Fe0.

Have in ore 22.8 " "

Want 20.1 " " or

30.4 lbs iron ore to be added.

30 : 15 = 32.2 : X, X = 16.1 lbs CaO necessary.

Have in the ore <u>11.8</u>

Want 4.3 lbs CaO or

8.7 lbs of limestone.

100 lbs lead ore requires.

30.4 " iron ore for fluxing SiO<sub>2</sub>

11.9 " " to furnish Fe for speiss and matte

8.7 " limestone

151.0 " charge per 100 lbs of lead ore, which gives 10 lbs of matte, and 10 lbs of bullion, hence have 151.0 -20 = 131.0 lbs of slag. Assume that the slag carries 1.5% S.  $131.0 \times .015 = 2.0$  lbs. Assume that the flue dust is 3.5% of the ore charge and that the dust carries 6.23% S. then S in flue dust =  $159.0 \times .035 \times .0623 = .32$  lbs S.

S in matte = 2.881bs.

S " slag = 2.0 (Iles Pb. Smelt. p 131)

S " dust = 0.3 " " " 150)

\$ burned off <u>1.7</u> or 25%

Total \$ 6.8 lbs in 100 lbs of ore.

Want each charge to weigh 1500 lbs. This shall consist of slag

	6.		
Slag	200#		
Ash	26.1		
Iron ore for	ash 10.4		
Limestone "	# 5.8	242.3	
Bead ore ar	nd flux	1257.7	
		1500.0	

151.0 $\dot{\mathbf{X}} = \frac{12}{1267.7}$ lbs.,	) = $8.3$ , then the full charge will be -
Lead ore	830 lbs (100x 8.3)
Iron ore for flux	256.4 " (30.9x 8.3)
" " As-S	99. " (11.9x 8.3)
Limestone	<u>.72.2</u> " (8.7 x 8.3)
	1257.6 "

We want to menelt 100 tons of ore per day. Since the iron flux carries values we include it under this classification, as ore, hence the ore per charge of 1500 lbs is 830 lbs. lead ore

> <u>366</u> " iron " 1196 " ore

100 tons = 200,000 lbs

200,000 1196 = 168 charges per day of 24 hours.

Mater	ial		Sic	$\mathbf{F} \boldsymbol{\epsilon}$	FeO		CaO '
Name Coke Ash	Dry Weight 26.1	<b>%</b> 40.3	1bs 10.5	% 26.5	1bs. 6.9	% 8.9	153. 2.3
Slag	200.0	30.0	60.0	40.0	8 <b>0</b> 00	15.0	30.0
Lead Ore	830.0	32.2	266.6	22.8	189.2	11.9	07.0
Iron " for Pb"256. " Ash 10. Iron ore fo As-S	$\begin{bmatrix} 5 \\ 8 \\ 266.9 \\ 99.0 \end{bmatrix}$	5.3	19.4	<pre>{73.1 0.0</pre>	195.1 0.0	3.1	11.3

Limesto	ne <sup>.</sup>	Dry Weight	%	lbs	ø	lbs.	7	<b>#</b> bs
for ore "ash	72.2 5.8	78.0	3.7	2.0	4.5	3.5	49.2	38.4
Factor		1500.0		385.6		475.0		179.9
40÷47851 ≝.084				30.09		40		15.1

Dimensions	of	the	Furnace
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In order to determine the inside of the furnace it is necessary to assume that, when Sull, the furnace will hold about 54 charges. The total weight of these charges will be

200 lbs slagn \$ 54 = 10800 lbs.

830 " ore **x** 54 = 44820 "

366 " iron ore \$54= 19760 "

78 " limestone x54 = 4212

210 " coke X54 <u>=11340</u> '

**Total** 97932

1 cu. ft. slag weighs 120 lbs (est.)
1 " " hematite broken 150 " (Richards Ore Dressing)
1 " " limestone weighs100 " " " "

Ħ

1 " " coke " 30 " " " "

1 " " ore " 119 " calculated as follows.

The weight of one cubic foot od lead ore was calculated from Vezin's rule(Richards Ore-Dressing)page 1190) as follows:

14% PbS X Sp. Gt.7.5 = 1.066.6" FeS X 72.6 = 0.1717.04%Fe203 and Be304X 5.0 = .9511.8% Ca0 X Sp. Gr. 2.7(est)=.2236.4% Si02 X "2.6 = .93

3.33

 $3.33 \times .57 = 1.89$ 62.5 X 1.9 = 118.7 lbs/jcu.ft.of ore.

Volume	of	limestone	in	the	furnace <u>4212</u>	= 42.12 Cu.Ft.
\$ <b>9</b>	Ħ	coke	Ħ	Ħ	100 " <u>11340</u>	= 376 00 ``
**	TŤ	iron ore	#	Ħ	30 " <u>19760</u>	= 131 00 ··· ^·
**	##	slag	Ħ	11	150 <b>"</b> _10800	= 90.00
Ħ	Ħ	lead ore	11	11	" <u>44820</u> 119	= 376.40
Tota	al v	of of	11	**	in cu ft.	= 1015.00 ~~

Assume the width at the tuyers as 42", height of ore columne 16' height of feed floor above tuyers 20', bosh of water jacket 18" height of water jacket above the tuyers 4'10", bosh of furnace walls above **jacketthe**simes walls at the ends of the furnace are boshed the same as at the sides but the water jackets are straight.

Area  $\mathbf{A} = \frac{5'5'/3'' + 5'}{2} \times 1/2'' = 58.48sq ft.$ Area  $\mathbf{B} = \frac{5' + 3.5'}{2} \times 2.41' = 22.48sq ft.$ Bosh at the ends, = av width X height X 10''  $5'.82''_3'' \times 13' ...'' \times 10'' = 63.6 cv. ft.$ Volumne for the rest of the furnace  $\mathbf{H}$ 1015-63.6 = 951.4 cu ft.

End area of the furnace = 22.48+ 58.12 = 80.6 sq. ft. Length = 951.4÷ 80.6 = 11.8' = 141.6"

Volumne of gases given ogg and of air supplied. We want to smelt 100 tons of ore per day, which requires 168 charges. S in one charge.

In ore 56.4 " coke .5 56.9#

Assuming 1/4 the total S burns off we have for one day

 $\frac{56.9 \times 168}{4} = 2389.8 \text{ lbs S burned to S}$ 

2389.8 lbs  $0_2$  giving 4779.6 lbs SO<sub>2</sub> (since the molecular weights of S and O are equal)

Assume that two thirds of the ZnS is burned off to ZnO then

 $2/3 = 1.6X 8.3 \times 168$  16 = 328.8 lbs 02 needed to form Zn0 ( 8.3 is the factor by which a 100 lb charge is increased to 1500 lbs).

In a 100 lb charge we have 2.3 lbs PbS going into the matte, hence in 1500 lb charge we have 2.3 X 8.3 # 19.09 lbs PbS in the matte.830 lbs. lead ore carries 14% PbS or 116.2 lbs. 116.2 lbs

PbS in matte 19.09

PbS to be reduced = 97.11 lbs. PbS is furst reduced to PbO or 97.11 lbs PbS becomes 90.6 lbs PbO and contains 6.47 lbs  $0_2$  thus

240: 16 = 97.11 : X, X = 6.47 97.11 - 6.47 = 90.6 lbs. Pb0 since the automic weight of 0 is 1/2 that of S.

6.47 X 168 # 1086.7 lbs 02 needed for this reaction. 0 needed to burn 6.6 lbs FeS to FeO = 1.2 lbs. hence for one day 1.2 X 8.3 X 168 = 1671.3 lbs 02

9.

210 lbs of coke carries 177.7 lbs of fixed carbon ( 210X 84.2%) Assume that 40% of this C burns to CO and 60% to CO<sub>2</sub>

 $177.7 \times 168 = 298541bs C_{\bullet}$ 

40% of this requires 1592/lbs 02 forming 27862 lbs CO.

29854 X.40X4/3 = 15921 lbs  $\theta_2 \left(\frac{16}{12} = \frac{4}{3}\right)$  forming 15921+11941 = 27862 lbs of CO.

Likewise

29854 X .60 X 8/3 = 47756 lbs  $0_2 \frac{32}{12} = \frac{8}{3}$  ) making 65665 lbs  $CO_2$ Total  $\Theta_2$  needed for the coke = 15921+47756 = 63677 lbs.

Summary.

02	needed	to	burn	s to	S <b>0</b> 2	per	day	2389	lbs.
Ħ	Ħ j	55 <b>8</b>	#1	Zn 📍	ZnO	*	**	329	*
Ħ	*	**	Ħ	Pb "	P <b>b</b> 0	Ħ	Ħ	1087	#
Ħ	**	H		40%C"	Co	Ħ	Ħ	159 <b>21</b>	Ħ
Ħ	**	#	#	₽e "	Fe0	Ħ	#	1671	Ħ
W	Ħ	#	Ħ (	60% <b>C</b> *	co <sub>2</sub>	**	Ħ	47756	#

Total  $0_2$  needed " " 69153 " or N2 "  $-\frac{77}{23}$  # 69153= 231524 lbs. 48.00 lbs per minute  $0_{2.\Lambda}$  23

 $32X \ 22.22 \ X \ \frac{48.00}{2} = 17065.0 \ cu \ ft. \ 0_2 \ per minute at standard pressure 760 mm or 29.93". Pressure at Denver is 25.5" hence at that altitude 17065.0 cu ft. becomes <math>\frac{29.93}{25.5} \ x \ 17065.0 = 20017 \ cu \ ft. \ at \ 0^{\circ}C.$  At 12°C volumme = 20017 (  $1 + \frac{12}{273}$  ) = 20898 cu ft.

 $N_2$  by vol.  $=\frac{79}{21}$  X 20898  $=\frac{78575}{78575}$  " "

Total vol. of air per minute= 99473 " "

### Size of Tuyers.

At 30 degrees F. 1 cu. ft of air weighs .0868 lbs at sea level. At 32 degrees F. or 0 degrees C. it weighs .0868  $\frac{2}{461} \times .0868$ ) or .0864 lbs. Pressure at Denver is 25.5 hence one cu. ft. of air in that locality weighs .0864 X  $\frac{25.5}{29.93}$  or .073 lbs.and one cu. ft. of water weighs

<u>62.32</u> .073 or 846 times as much as one cu. ft of air.

Assume 2.6 sq. ft. hearth area for each tuyers. Number of  $\frac{42X \ 141.6}{144X \ 2.6} = 16. \text{ Air per second per tuyer} = \frac{99473}{60 \ X \ 16} = 103.6$ tuyers equal cu ft.

Let the area of a tuyer be y sq. ft. Let the pressure be 2 lbs. per square inch = 2 X 144 ŷ 1bs. per tuyer, then 12: X = 62.32 : (2 X 144 y), X = water guage reading, = 55.44 y inches.

The pressure of a column# of water 55.44 y inches high is equivalent to that of an air columns 3908.5 feet high, thus:  $55.44 \text{ y} \times 846 = 3908.5 \text{ y}$ At 12 degrees C it is equivalent to 3908.5 y  $\times \frac{285}{273}$  or 4064.8 y feet = h.  $V = \sqrt{2 \text{ gh}} = 8\sqrt{4064.8 \text{ y}} = 509.6\sqrt{\text{y}}.$ 

Area = volumme + velocity or y = 103.6509.6  $\sqrt{y}$ , y = .089 sq ft. or

12.82 sq. in. Diameter of tuyers = 4.0 inches.

Oxygen furnished within the charge itself.

From the slag table we have 6.9 lbs FeO+195.1 lbs. FeO in the ash and flux for the ores = 202.0 lbs. 2 FeB : 0 = 144 : 16 = 202.0 :X **X** = 22.4 lbs.0. This oxygen is given off by

Fe<sub>2</sub>0<sub>3</sub> in being reduced to FeO by C.

0 given off by Fe<sub>2</sub>0<sub>3</sub> in forming speiss and matte is determined as follows: since the iron ore contains 81% Fe B, of 99 lbs of ore =80.2# Fe203. 0 in 80.2 lbs Fe  $P_3 = 24.06$  lbs, thus 160 : 48 = 80.2 f X, X = 24.06 Total oxygen given off from one charge = 22.4+24.1 = 46.5 lbs 02

For 168 charges we have 46.5 X 168 # 7812.9 1bs. 0,

O furnished by iron oxide in the lead ore.

Ore contained 6.6 lbs FeS.

### 17.04 " FeO from slag table

(1) Assume 2/3 of the FeO came from  $Fe_2O_3$  of the roasted ore.

(2) and 1/3 from  $Fe_30_4$ 

(1) 144 : 16 = 11.36 : X,  $x \neq 1.26$  lbs  $0_{\cancel{2}}$ 

(2) 216 : 16 = 5.68 : X ,X# <u>.42</u> " "

Available  $0_2$  in lead ore =1.68 "/100 lbe ore which is given off when the higher oxides are reduced to FeO.

1.68 X 8.3 X 168 = 2342 lbs 02 per day.

CO, given off from the charge.

In 100 lbs charge we use 8.7 lbs limestone, containing 75.5 % CaCO  $_3$ 

10.3% MgC03 7.2% FeC03, hence

6.6 lbs  $CaCO_3$  gives 2.9 lbs  $CO_2$ 

.9 " MgCO<sub>3</sub> " 0.5 " " .6 " FeCO<sub>3</sub> " <u>0.3</u> " " 3.7 " "

3.7 X 8.3 X 168  $\pm$  5157.2 lbs CO<sub>2</sub> given off from one day's run. All the oxides that were reduced were assumed to be reduced by CO though in practice some of  $\frac{them}{14}$  are reduced by Calone, but figures from actual practice were not obtainable, and probably would not effect the calculations to a very great extent anyhow.

Total O given up by iron oxides 7812

2342

10154 lbs 02

This requires 17769 lbs CO to form CO2, thus

28: 16 = X ; 10154, X = 17769

 $\begin{array}{rcl} & \text{CO}_2 & \text{formed} = 17769 \pm 10154 = 27923 & \text{kbs.} \\ & \text{CO} & \text{to reduce 1087 lbs 0 from Pb0, } & \frac{7 \times 1087}{4} = 1902 & \text{lbs.} \\ & \text{CO} & \text{formed by burning coke at the tuyers} & 27862 & \text{lbs.} \\ & & \text{CO} & \text{to reduce iron oxides 17769 lbs.} \\ & & & & \text{lead} & \underline{1902, 19671} \\ & & & & & 8291 & \text{lbs.} \end{array}$ 

Summary of Furnace Gases Passing Through Stack.

Oxygen furnished within the charge.

From	Fe <sub>2</sub> 03	in	iron	ore	and	ash	7812 lbs
#	#	Ħ	lead	"}			9349 #
<b>#</b>	Fe 0 3 4	Ħ	11	")			20 <b>-</b> 20
#	P <b>b</b> 0						1087 "
							11241 #

This oxidizes CO to  $CO_2$  and therefore is not to be deducted from  $O_2$  furnished at the tuyers.

11241 lbs 02 require <u>s 19671</u> <b>k</b> bs CO 196	71
	,
CO <sub>2</sub> formed by above 30,712 165	
" given off by carbonates <u>5,157</u>	

Total CO passing through unchanged 8291 lbs.

55230

Total weight of gases leaving stack :

SO2	<b>4779 lbs</b>	1.61%
N <sub>2</sub>	231524 "	77.22"
<b>c</b> 0	8291 "	2.65"
<b>c</b> o <sup>2</sup>	_5523 <b>0</b> _ "	18.42"
	299824 "	

Total CO2

4779 lbs S0<sub>2/ day</sub> means 3.3 lbs per minute 0z = molecule = 64  $64x 22.22 \times \frac{3.3}{2}$  (64 oz = 21bs) 231524 lbs N<sub>2</sub> per day or 1608 lbs (280z = 1.75 lbs) per minute 28X 22.22X <u>1608</u> lbs 1.75 hs

13.

8221 lbs C0 per day, or 5.7 lbs per min. 28X 22.22 X 5.7 1.75 2026 2.58 755230 lbs C0<sub>2</sub> per day, or 38.2 lbs " " 44 oz X 22.22 X  $\frac{38.3}{2.75}$  (44 oz=2.75lbs) 13944 77565

The accompanying drawings are self explanatory. The details fixed by practice were derived from a blue print of a Lead Blast Furnace furnished by the Denv r Engineering Works.