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1907

Design of a lead blast furnace

Walter Irving Phillips

Andrew Jackson Seltzer

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Department: Chemistry; Materials Science and Engineering

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FOR THE

Degree of Bachelor of Science

IN

Chemistry and Metallurgy.

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SUBJECT,

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"Design of a Lead Blast Furnace."

WALTER I. PHILLIPS. A. J. SELTZER. JUNE, 1907.

DESIGN OF A 100 TON LEAD BLAST FURNACE.

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Calculations for the charge. Calculations for the inside dimensions of Furnace. Calculation of the Furnace gases. Calculation of the size of the tuyers. Drawings of the Furnace.

In order to ket the approximate size of the Furnace we made the following assumptions, being guided as far as possible by the practice of the Globe Smelting Works at Denver, Colorado whenever that could be ascertained.

The coke used is that made at Tuscarawas. Ohio. and has the following composition: water 0.13%, volatile matter 2.75%, fixed carbon 84.2%. ash 12.4%, sulphur 3.7%. It was assumed that the S. was distributed thus: in volatile matter 1.8%, in ash 1.8% as FeSpand CaSO4.

The ash analysed as follows: SiO₂ 40.3%, Fe₂O₃ 29.4%, CaO 6.0, Mg0 1.4%, A1203 20.1%, FeS2 and GaS04 1.8%

The lead ore delivered to the furnace comes from Leadville and has been previously roasted flown to 6.8% and its composition is

Fes Fe_5O_3 MnO CaO MgO ZnS Al_2O_3 As PbS Cu₂S 510_o 36.4 6.6 19.3 4.3 4.4 5.26 2.4 2.5 5 14.0 1.83 Au Λg.

 $50.50z.$ Trace.

The iron ore is a dry oxidized silver ore from isadville, Colo., of the following composition:

In order that these metals shall enter the slag they must become oxides, and iron will enter the slag only as FeO hence the other oxides of iron will have to be calculated over to that oxide when figuring up the charge for the furnace. These calculations are made by means of simple ratios of atomic weights and will not be gone into in detail further than to give one example; thus, to determine the amount of FeO in -19.3# FegO3of the lead ore we have:

 Fe_2O_3 : 2FeC = 160: 144 = 19.3# : X $X = 17.4#$ FeO in 100 lbs of ore. The 6.6 lbs FeS burned to FeO = 5.4 lbs. FeO. Total Feo = $17.4+$

 $5.4 = 22.8$ lbs FeO.

In this manner the following table of adjusted oxides was obtained:

Since MnO acts much like FeO in the slag, it is counted as FeO in the adjusted table. Its atomic weight is so near that of FeO that no appreciable error was introduced by adding the weight of the two oxides directly without figuring them over from their atomic weights. MgO acts like CaO in many respects hence it is counted as lime in the table. The weights were figured however from the atomic weights thus:

multiply the weight of MgO in the ore by 1.4 to get the equivalent weight of GaO for combining with SiO₀.

The slag to be calculated is to be 30- 40- 15, which will be liquid, fairly easily fusible at a low temperature and at the same time decrease the amount of barren limestone put into the charge. IRON ORE CALCULATIONS. When buying iron ore for fluxing purposes only the "available" iron is paid for, i.e. the SiO_o in the flux is not wanted hence the FeO, needed to slag this silica, is deducted before paying for the flux.

In 100 lbs. of ore we have 66 lbs FeO available. This result $\mathbf{1}$ was obtained as follows:- slag is to be $50 - 40 - 15$, hence

30 : 40 = 5.8 : X, or X = 7. \$# Fe0 to slag 5. 3# SiO₀

73.1 - 7.1 = 66.0# FeO available. This 66.0 lbs Feo. carries 51.1 1b Fe.

Xo determine how much lime should be added we used the following proportion:

30 : 15 = 5.3 : X. X h 2.6 lbs. CaO. The iron ore carries 3.1 lbs CaO hence it is self fluxing as regards lime.

11 IRON FOR SPEISS. As. is very undesirable in the lead bullion, and if it is present in the ore it must be provided for. Iron forms several alloys with As but the only one which is liquid when fused is FegAs. This is termed "Speiss" and goes with the matte, in the furnace, thus preventing the As from going into the Lead. In 100 lbs. of lead ore we have .5 lbs As. The iron needed for speiss is thetained thus:

 $(5x 56) : 75 = X : .5, X = 1.9$ lbs Fe.

100 lbs iron ore 51.1 = \ddot{x} : 1.9, \ddot{x} = 3.71 lbs. $\ddot{\circ}$ iron ore necessary to form the speiss for 100# lead ore. IRON FOR MATTE. The Matte fall should be kept low as considerable lead will otherwise go into it.

 \mathbb{Z}^n

3.

The matte fall was calculated at 10% and its composition was assumed as follows:

In 10 1bs matte have

.38 Lbs. S from 1.88 lbs Cu.S $"2.30"PbS$ $.30$ H H H 5.82 H FeS . $2,12$

" 10.00 " matte. -2.80 \mathbf{H} \mathbf{H}

5.82 lbs FeS consains 3.7 lbs Fe which is equivalent to 7.2 1bs iron ore.

IV. COKE-ASH CALCULATIONS. . Use12.4% Tuel. Charge to be 1500 lbs 12.4%X 1500 =210 lbs coke containing 26.1 lbs. ash composed of the following SiO₂ FeO CaO $10.5# 6.9$ 2.3

30 : 40 = 10.5 : X, X= $\frac{4}{10}$ 105 Fe0

FeO present in ash 6.9

 7.1 lbs = 10.8 lbs. iron ore. heeded 30: $15 = 10.1$: $X = 5.05$ lbs CaO needed for 10.5 lbs SiO₂ CaO present in the ash = 2.3#, CaO needed = 5.05 \approx 8.3 = 2.75 lbs CaO or 5.5 lbs limestone.

V. LEAD ORE.

4.2 lbs SiO₂ go to the matte, 100 lbs ore carries 36.4 lbs. $Si0_2$, $Si0_2$ to be fluxed = 36.4 - 4.2 = 32.2 lbs.

 $30:40 = 32.2: X$, $X = 42.9$ lbs FeO.

Have in ore 22.8 "

 20.1 μ * or Want

30.4 lbs iron ore to be added.

30 : 15 = 32.2 : X, X = 16.1 lbs CaO necessary.

Have in the ore 11.8

Want 4.3 lbs CaO or

8.7 lbs of limestone.

100 lbs lead gre requires.

30.4 " iron ore for fluxing SiO₂

 11.9 $''$ Ħ " to furnish Fe for speiss and matte

8.7 " limestone

151.0 " charge per 100 lbs of lead ore, which gives 10 lbs of matte, and 10 lbs of bullion, hence have 151.0 -20 = 131.0 lbs of slag. Assume that the slag carries 1.5% S. 131.0 X.015 = 2.0 1bs. Assume that the flue dust is 3.5% of the ore charge and that the dust carries 6.23% S. then S in flue dust = 150.0 x .035 x .0623 = .32 lbs S.

S in matte = 2.81 bs.

 S * slag = 2.0 (Iles Pb. Smelt. p 131)

 S ***** dust = 0.3 $"$ $150)$

 $$$ burned off 1.7 or 25%

6.8 lbs in 100 lbs of ore. $Total S$

Want each charge to weigh 1500 lbs. This shall consist of slag

We want to ment 100 tons of ore per day. Since the iron flux carries values we include it under this classification, as ore, hence the ore per charge of 1500 lbs is 830 lbs. lead ore

> 366 $''$ iron " 1196 $''$ ore

100 tons = $200,000$ lbs

 $200,000$ 1196 = 168 charges per day of 24 hours.

 $3.33 \times .57 = 1.89$ 62.5 X 1.9 = 118.7 lbs/cu ft of ore.

Assume the width at the tuyers as 42", height of ore columne 16' height of feed floor above tuyers 20', bosh of water jacket 18" height of water jacket above the tuyers 4'10", bosh of furnace walls above iackstthe"siles walls at the ends of the furnace are boshed the same as at the sides but the water jackets are straight.

Area $\mathbf{A} = \frac{5.5\frac{1}{3} + 5.5\frac{1}{3}}{2}$ \times 1/2" = 58.48sqft.
Area $\mathbf{B} = \frac{5.45.5 \times 2.41.5}{2}$ \times 2.48sqft.
Bosh at the ends, = av width X height X 10" A 5.8% "x /3' \cdot " x /0" = 63.6 cu. ft. Volumne for the rest of the furnace # 1015-63.6 = 951.4 cu ft. B

End area of the furnace = $22.48 + 58.12 = 80.6$ sq. ft. Length = $951.4 \div 80.6 = 11.8' = 141.6''$

Volumne of gases given ogg and of air supplied. We want to smelt 100 tons of ore per day, which requires 168 charges.

S in one charge.

In ore 56.4 \bullet coke \bullet \bullet \bullet 56.9#

Assuming 1/4 the total S burns off we have for one day

56.9 X 168 $\frac{9 \text{ X } 168}{4}$ = 2389.8 lbs S burned to S θ_2 which requires

2389.8 lbs $0₂$ giving 4779.6 lbs $S0₂$ (since the molecular weights of S and O are equal).

Assume that two thirds of the ZnS is burned off to ZnO then

 $2/3 = 1.6X 8.3 X 168$ $16 = 328.8$ lbs 02 needed to form 1 65 ZnO (m.3 is the factor by which ^a 100 Ib charge is increased to 1500 $1bs$).

In a 100 1b charge we have 2.3 lbs PbS going into the matte, hence in 1500 lb charge we have $2.3 \times 8.3 \times 19.09$ lbs PbS in the matte.830 lbs. lead ore carries 14% PbS or 116.2 lbs. 116.2 Ibs

PbS in matte 19.09

PbS to be reduced $= 97.11$ lbs. PbS is furst reduced to PbO or 97.11 lbs PbS becomes 90.6 lbs PbO and contains 6.47 lbs $0₂$ thus

 $240: 16 = 97.11 : X, \; \dot{X} = 6.47$ $97.11 - 6.47 = 90.6$ Ibs. PbO since the automic weight of ⁰ is 1/2 that of s.

6.47 X 168 \neq 1086.7 lbs 0₂ needed for this reaction. 0 needed to burn 6.6 lbs FeS to FeO = 1.2 lbs. hence for one day 1.2 X 8.3 X 168 = 1671.3 lbs 02

210 lbs of coke carries 177.7 lbs of fixed carbon (210X 84.2%) Assume that 40% of this C burns to CO and 60% to CO₂

177.7 X 168 = 298541bs C_6

40% of this requires 1592/1bs O₂forming 27862 lbs CO.

29854 X.40X4/3 = 15921 1bs θ_2 $\frac{16}{12} = \frac{4}{3}$ forming 15921+11941 = 27862 lbs of CO.

Likewise

29854 X .60 X 8/3 = 47756 lbs $0.2 \frac{132}{12} = \frac{8}{3}$) making 65665 lbs 0.2 Total θ_2 needed for the coke = 15921+ 47756 = 63677 lbs.

Summary.

Total 0₂ needed $\frac{77}{182}$ **#** 69153 **#** or
48.00 lbs per minute $\delta_{2.0}$ $\frac{77}{25}$ **#** 69153= 231524 lbs.

32X 22.22 X $\frac{4800}{2}$ = 17065.0 cu ft. O₂ per minute at standard pressure 760 mm or 29.93". Pressure at Denver is 25.5" hence at that altitude 17065.0 ou ft. becomes $\frac{29.93}{25.5}$ x 17065.0 = 20017 ou ft. at θ^{\bullet} C. At 12°C volumne = 20017 ($1+\frac{12}{273}$) = 20898 cu ft.

 N_2 by vol. $\frac{79}{21}$ X 20898 $= 78575$ $^{\prime\prime}$ $^{\prime\prime}$

Total vol. of air per minute= 99473 "

Size of Tuyers.

At 30 degrees F. 1 cu. ft of air weighs .0868 lbs at sea level. At 32 degrees F. or 0 degrees C. it weighs .0868- $\frac{2}{461}$ x .0868)or .0864 lbs. Pressure at Denver is 25.5 hence one cu. ft. of air in that locality weighs .0864 $X = \frac{25.5}{22.27}$ or .073 lbs.and one cu. ft. of water weighs

 $\frac{62.32}{073}$ or 846 times as much as one cu. ft of air.

Assume 2.6 sq. ft. hearth area for each tuyers. Number of $\frac{42X \t141.6}{144X \t2.6}$ 16. Air per second per tuyer $\frac{99473}{60 \t16}$ = 103.6 tuyers equal cu ft.

Let the area of a tuyer be y sq. ft. Let the pressure be 2 lbs. per square inch = 2 X 144 \hat{y} 1bs. per tuyer, then 12: X = 62.32 \hat{x} (2 X 144 y), $X =$ water guage reading, = 55.44 y inches.

The pressure of a columny of water 55.44 y inches high is equivalent to that of an air columns 3908.5 feet high, thus: $\frac{55.44 \text{ y}}{12}$ χ 846 = 3908.5 y $V = \sqrt{2gh} = 8\sqrt{4064.8} y = 509.6\sqrt{y}$.

Area = volumne + velocity or $y = \frac{103.6}{509.6 \sqrt{y}}$, $y = .089$ sq ft. or

12.82 sq. in. Diameter of tuyers $= 4.0$ inches.

Oxygen furnished within the charge itself.

From the slag table we have 6.9 lbs FeO+195.1 lbs. FeO in the ash and flux for the ores = 202.0 lbs. 2 FeD: $0 = 144$: $16 = 202.0$: X $x = 22.4$ lbs.0. This oxygen is given off by

 $Fe₂O₃$ in being reduced to FeO by C.

0 given off by Fe_0O_τ in forming speiss and matte is determined as follows: since the iron ore contains 81% $\texttt{Fe}_{2}\texttt{P}_{3}$ of 99 lbs of ore =80.2# 0 in 80.2 ibs $\text{Fe}_{2}\text{O}_{3}$ = 24.06 lbs, thus 160 : 48 = 80.2 f X, X = 24.06 Total oxygen given off from one charge = $22.4 + 24.1 = 46.5$ lbs $0₂$

For 168 charges we have 46.5 X 168 # 7812.0 lbs. 0_{ϕ} .

O furnished by iron oxide in the lead ore.

Ore contained 6.6 lbs FeS.

17.04 " FeO from slag table

(1) Assume $2/3$ of the FeO came from $Fe₂O₃$ of the roasted ore.

(2) and $1/3$ from $Fe₃O₄$

(1) 144 : 16 = 11.36 : X, $x = 1.26$

(2) 216 : 16 = 5.68 : X, X^{*} .42

Available 0_2 in lead ore =1.68 "/100 lbe ore which is given off when the higher oxides are reduced to FeO.

1.68 X 8.3 X 168 = 2342 1bs 0_{2} per day.

CO₂ given off from the charge.

In 100 lbs charge we use 8.7 lbs limestone, containing 75.5 $\%$ CaCO₃

10.3% $MgCO_{3}$ 7.2% FeCO₃, hence

6.6 lbs $CaCO₃$ gives 2.9 lbs $CO₂$

.9 $MgCO₃$ $M_{O.5}$ m $.6$ **H** $FeCO_{\rm Z}$ **H** 0.3 **H H** $3.7 \cdot$ $\prime\prime$..

3.7 X 8.3 X 168 $\#$ 5157.2 lbs CO₂ given off from one day's run. All the oxides that were reduced were assumed to be reduced by CO them are
though in practice some of $\frac{1}{2}$ reduced by $\frac{1}{2}$ calone, but figures from actual practice were not obtainable, and probably would not effect the calculations to a very great extent anyhow.

Total 0 given up by iron oxides 7812

2342

10154 1bs 0_p

This requires 17769 lbs CO to form CO_2 , thus

28: 16 $= x_{i}$: 10154, X = 17769

 $CO₂$ formed = 17769 + 10154 = 27923 kbs. C^d to reduce 1087 1bs 0 from Pb0, $\frac{7 \times 1087}{4}$ = 1902 lbs. CO formed by burning coke at the tuyers 27862 lbs. CO to reduce iron oxides 17769 Ibs. lead 1902, 19671 CO passing unchanged to stack 8291 lbs. Summary of Furnace Gases Passing Through Stack.

Oxygen furnished within the charge.

This oxidises CO to CO₂ and therefore is not to be deducted from ⁰2 furnished at the tuyers.

Total CO passing through unchanged 8291 lbs.

Total weight of gases leaving stack

4779 lbs $SO_{2/}$ day means 3.3 lbs per minute $0z$ \rightarrow molecule = 64 $64X$ 22.22 $X \frac{3.3}{8}$ (64 oz = 21bs) 231524 lbs N_2 per day or 1608 lbs
(28oz = 1.75 lbs) per minute 28X 22.22X 1608 1bs 1.75 cu ft. 4346 5% */* 5θ 57150° A 5.55 \sim $i^{3}./J$ ~{ii'O

13.

8201 lbs CO per day, or 5.7 lbs per min. 2.58
17.95 PBX 22.22 $X = \frac{5.7}{1.75}$ 2026 ≤ 55930 lbs $C0_{2}$ per day, or 38.2 lbs " " 44 oz X 22.22 X $\frac{38.5}{2.75}$ (44 oz=2.751bs) 13044 77568

The accompanying drawings are self explanatory. The details fixed by practice were derived from a blue print of a head Blast Furnace furnicled by the Denv r Engineering Works.