

1910

## A study of the efficiency of discharge of classifier spigots

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THESIS

Degree of Bachelor of Science.

A STUDY OF THE EFFICIENCY  
OF DISCHARGE OF CLASSIFIER SPIGOTS.

*T 210*

10913

By

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Approved

*Boyd Dudley, Jr.* May 20, 1910.

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A knowledge of the amounts of water and sand that will be discharged by classifier spigots under various conditions is of considerable importance in the design of classifiers. Suppose it is desired to discharge fifty tons of sand with an average diameter of 2 m.m. through a spigot orifice, the sand being mixed with 100 tons of water and the entire amount of the mixture being discharged in ten hours from the spigot, which is submerged to a depth of two feet under the water. How large a spigot is required? Problems such as this are by no means uncommon. While in many cases they may be solved by guess and trial, still the knowledge of even a limited amount of data on the subject would materially increase the accuracy of guesses and decrease the number of trials necessary to a solution of the particular problem. It was with the idea of securing such data and determining the influence of various factors upon efficiency of discharge of classifier spigots that this investigation was started.

The efficiency of discharge of a spigot for mixtures of water and sand is governed by many variables, some important and others relatively unimportant. Apparently among the most important

are the following, the particular design of the spigot and the character of the column through which the pulp passes before reaching the spigot, the ratio of the size of ore grain to the size of the spigot orifice, and the ratio of water to sand in the pulp. Owing to the lack of time only one particular design of sorting<sup>column</sup> was studied. Therefore no conclusions were reached in regard to this factor. The influence of the ratio of the diameter of ore grain to the diameter of the spigot orifice was considered only incidentally. The effect upon the efficiency of varying the ratio of water to sand was given the greatest amount of attention, and all of the experiments were performed with a view of securing information on this point.

The arrangement of the apparatus, which consists of a classifier, two launders, spigots, and suitable support, is shown in Plate I.

The classifier was made of galvanized iron, the upper part being cylindrical in shape having a diameter of 16 inches and <sup>a length of</sup> ~~extending~~ 18.6 inches, terminating in a cone of 60 degrees, at the apex of which was attached a cylinder 4 inches in diameter and extending 12 inches making a total height of 46.6 inches. At one metre distant from

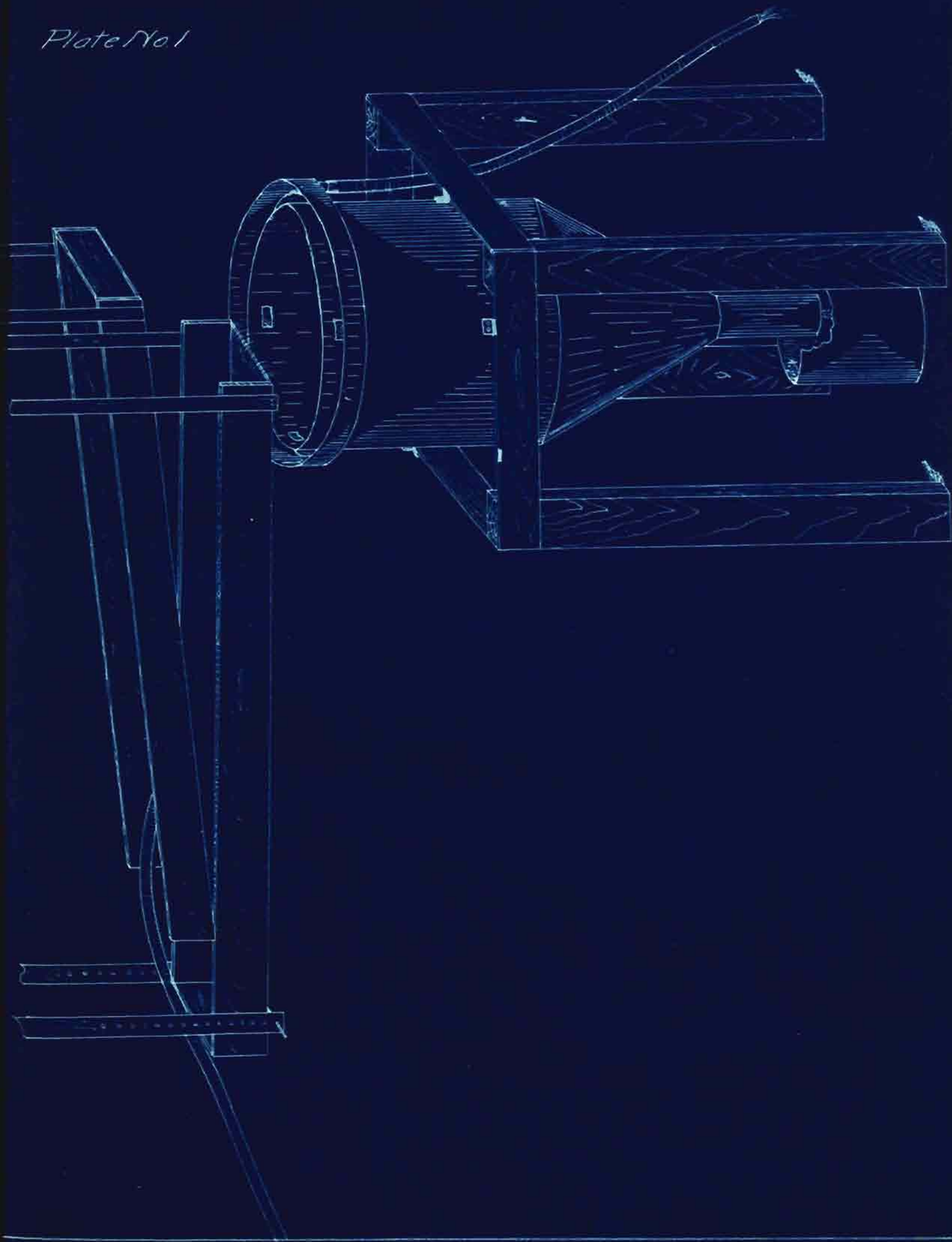
the bottom slots were cut in the classifier which allowed the excess water to overflow into a launder which encircled the classifier. Attached to the sides of the classifier <sup>were</sup> angle irons which served as supports. A section of the classifier is shown in Plate II.

The spigots were made of soft wood, a glass tube being fitted into the perforated wooden plug. All of the tubes were cut with their length four times the diameter in order to eliminate any influence that a variable ratio of length to diameter might exert upon the discharge efficiency of the spigot. The remainder of the wooden plug was coned to an angle of 60 degrees, the total length of the spigot varying with the length of the glass tubing used. Four spigots in all were used, the diameters being as follows: 1.83 m.m., 6.3 m.m., 9.1 m.m., and 14.3 m.m. The spigots were inserted into the small cylinder of the classifier and made water tight by means of paraffine.

The two launders were made of wood, rectangular in shape and closed at one end.

The classifier was supported by means of a wooden frame work <sup>The drawing of</sup> which is self explanatory.

Plate No 1







The first thing we did after getting the different parts of the apparatus was to assemble them in the most convenient manner, a sketch of the same is shown in Plate III.

The material used was a clean chert (Sp.Gr. 2.56) being sized through accurately measured screens, the average size grains being 0.373 m.m., 0.606 m.m., 0.855 m.m., 1.461 m.m., 2.972 m.m., and 4 m.m. in diameter respectively.

By experiments carried on by other parties, it was found that if a bank of ore was kept in a launder the water passing through would saturate itself with a constant amount of the ore and no more, this amount, however, varying with the slope of the launder and <sup>with the</sup> ~~on~~ amount of water used. This principle was adopted by us in this research work, <sup>and the classifier was fed by allowing the water to carry</sup> This was found to be <sup>sand down the</sup> ~~classifier~~ <sup>launder,</sup> better than an automatic shaking feeder in that the amount of sand was kept approximately constant at each slope and also was much easier to feed. The two launders used were placed one above the other and sloping in opposite directions. The reasons for using two launders were twofold, first, to break the impulse of the water so that there would be no undue pressure on the surface of the water in the classifier directly underneath the spillway of the

lower launder, which fed material to the classifier; and, second, so that we could handle the feeding of the sand much better in the lower launder, where the water current was uniform, than if just one launder was used for feed water and also as a place for feeding the sand.

The spigot was closed and the classifier filled with water, no sand being fed in during this operation. When the classifier was filled up to a certain point, this being one metre distant from bottom of spigot, the sand was then fed into the launder. It may be stated here that the sand was run through the classifier once in order to saturate it with water, for it proved by experiment that less amount of pulp (sand and water) issued from the spigot in the same length of time when the sand was dry, <sup>than</sup> and when the sand was wet, the same size sand, same slope, and same spigot being used. The sand was fed into the launder and when the pulp was coming out of the spigot at a uniform rate, it was deflected into a jar, the time being noted by means of a stop-watch. When the jar had become filled up to a certain point at or near one of the gauging points, the pulp was deflected into a refuse box, time again being noted. Before entering the refuse box, the pulp was passed over a screen, the sand remaining on the surface and the water passing through. The jar, the weight of which

was known, with its contents of pulp was carefully weighed. The weight of pulp was calculated by difference in weight. The volume of pulp was also recorded. The jar was cleaned and the experiment repeated, all variables remaining the same for two or more of these experiments, - the time, weight, and volume being recorded in each case. After a sufficient amount of data had been taken <sup>with</sup> ~~on~~ one slope, <sup>one</sup> ~~same~~ size <sup>of</sup> sand, and <sup>one</sup> ~~same~~ size <sup>of</sup> spigot being used, the slope was then increased, <sup>the</sup> ~~same~~ routine as described above being followed. The slope was gradually increased until the amount of sand carried by the water was too much for the spigot to discharge without clogging. The lower launder was then dropped to the lowest slope and more data taken with different sized sand. When all the different sized sands were used that could be on one spigot, that spigot was taken out and another one put in. The same method of taking data was used on all spigots, a record of each being kept.

Using the data thus obtained, the results and method of calculation are given on the following page.

Wt. of jar and pulp - Wt.of jar = Wt.of pulp.

$\frac{\text{Wt.of pulp}}{\text{Seconds}} = \text{Wt.of pulp per sec.}$

$\frac{\text{Vol.of pulp}}{\text{Seconds}} = \text{Vol.per sec.}$

Let R = Ratio of water to sand by weight.

" p = Specific Gravity of pulp.

" d = Specific Gravity of sand.

Now consider "d" grams of sand discharged  
with "R" grams of water per second.

Let total weight discharged per sec. = W gms.

Then  $W = d + R$ .

Let total volume discharged per sec. = V cu.cm.

Since  $d + Rd = \text{Wt.of pulp}$

Then  $V = \frac{d + Rd}{p}$

But  $1 + Rd = V$

Therefore  $1 + Rd = \frac{d + Rd}{p}$

Hence  $R = \frac{d - p}{dp - d}$

Putting in value of p = 2.56

We get  $R = \frac{2.56 - p}{2.56p - d}$

The following table shows observed and calculated data, and a few words in way of explanation may make the table of data more clear.

The theoretical discharge on top and on bottom of spigots was calculated from the formula  $Q = a v$   
 $v = \sqrt{2gh}$ . Therefore  $Q = a\sqrt{2gh}$

$Q$  = Quantity of water.

$a$  = Area of the spigot.

$g$  = 980 (constant)

$h$  = Height (This being one meter in one case  
and one meter minus length of tube  
in the other.)

"a" was calculated for each spigot, diameter being known in each case.

The size of pulp is the size of the average grain in each case.

The efficiency was obtained by dividing the actual discharge by the theoretical, the theoretical discharge used being the one on the bottom of the spigot.

# — Data — The Efficiency Of Discharge Of Pulp Through Classifier Spigots Of Different Design.

## Derivation Of Formula.

Let  $p$  = Sp Gr. of Pulp =  $\frac{\text{Wt in grams}}{\text{Vol in cc}}$  or  $H_2O + \text{Ore}$  :  $d$  = Sp Gr. of Ore = 2.56  
 $R$  = Ratio Of Water To Ore By Weight.  $1 + Rd = \frac{d + Rd}{p}$   
 $p + Rd p = d + Rd$   $Rd p - Rd = d - p$   $\therefore R = \frac{d - p}{dp - d} = \frac{2.56 - p}{2.56xp - 2.56}$

THE HEAD IN ALL CASES = 1 METER

Area Of Spigot in sq cm	Diame. Spigot in mm	Head On Top Of Spigot	Time in Secs	Litres H <sub>2</sub> O Ore	Grams H <sub>2</sub> O Ore	"R"	Wt Pulp Per Sec.	Vol Pulp Per Sec.	Theoretical Discharge On Top	Theoretical Discharge On Bottom	Size Of Pulp	Eff.
263.02	18.3	927	144	12.75	13279.	1535	922.2	885.5	112116	1164.3	4 mm	76%
"	"	"	13	"	12485.	542	9609	861.5	"	"	"	74
"	"	"	133	1162	12212.	116	9180	873.5	"	"	"	75
"	"	"	141	1289	13336.2	1694	9462	914.2	"	"	2.972	78.5
"	"	"	165	124	14695.7	378	8907	751.5	"	"	"	64.5
"	"	"	136	1184	13052.5	1081	9596	870.5	"	"	"	74.7
160.6	14.3	943	205	1135	12312.7	2282	600.5	5830	686.5	708.3	"	85.3
"	"	"	216	1213	13241.6	674	6130	564.2	"	"	"	79.6
"	"	"	212	1228	13109.2	895	618.2	579.7	"	"	"	81.8
"	"	"	20	1228	12598.5	25.5	6300	6140	"	"	1461	86.6
"	"	"	20	1183	12655.2	876	6325	5910	"	"	"	83.4
"	"	"	219	1255	13563.2	74	619.2	573.0	"	"	"	80.9
"	"	"	241	1336	15492.7	362	642.7	554.7	"	"	"	78.3
65.03	9.1	9636	30	2.19	2270.	169	252.2	243.3	2524	287.7	"	84.5
"	"	"	10.0	244	2610.5	89	2610	2440	"	"	"	84.8
"	"	"	11.1	253	2894.2	54	2607	2279	"	"	"	79.2
"	"	"	9.8	245	2553.7	135	2606	2500	"	"	0.855	86.8
"	"	"	10.2	252	2780.7	662	2726	2471	"	"	"	85.9
"	"	"	14.7	250	3234.7	168	2201	170.0	"	"	"	59.1
"	"	"	9.7	243	2630.3	739	2712	250.5	"	"	0.606	870
"	"	"	10.7	256	2894.2	593	2704	238.7	"	"	"	82.9
"	"	"	12.8	276	3291.5	272	2571	214.3	"	"	"	74.4
"	"	"	13.0	257	3348.2	157	2575	197.7	"	"	"	68.7
"	"	"	9.7	247	2496.5	776	2573	254.6	"	"	0.373	88.8
"	"	"	9.6	242	2497.0	193	2601	252.1	"	"	"	87.6
"	"	"	10.5	268	2894.2	734	2756	255.2	"	"	"	88.7
"	"	"	11.0	265	2978.7	463	2708	240.9	"	"	"	83.7
"	"	"	11.5	266	3132.6	395	2724	2311	"	"	"	80.2
"	"	"	9.8	256	2576.5	1554	2628	261.3	"	"	0.173	308
"	"	"	9.9	255	2576.5	775	2602	257.6	"	"	"	89.5
"	"	"	9.7	247	2553.7	76.3	2632	254.7	"	"	"	88.5
"	"	"	10	256	2667.2	157	2667	256.0	"	"	"	89.0
31.17	6.3	9748	30	3.80	2497.0			123.3	"	"	"	89.8
"	"	"	21	247	2474.3	3116	1178	1176	1355	137.2	"	85.7
"	"	"	20.2	243	2440.2	1556	1208	120.3	"	"	"	87.7
"	"	"	216	25	2724	6.3	1261	1161	"	"	"	84.6
"	"	"	20.7	247	2553.7	764	1234	119.3	"	"	0.373	86.9
"	"	"	21.4	256	2605.9	385	1218	119.6	"	"	"	87.1
"	"	"	21.2	246	2655.9	3116	1253	120.7	"	"	"	87.9
"	"	"	21.1	251	2667.2	998	1264	118.9	"	"	"	86.6
"	"	"	23.5	249	3007.7	341	1280	110.2	"	"	"	80.3
"	"	"	20.4	251	2512.7	1556	123.5	123.1	"	"	0.606	89.7
"	"	"	21.2	258	2633.2	308	124.2	121.7	"	"	"	88.7
"	"	"	21.4	249	2667.2	826	1246	116.9	"	"	"	85.2
"	"	"	23.3	256	2905.6	419	124.7	109.8	"	"	"	80.0
"	"	"	20.4	259	3268.8	193	128.7	101.9	"	"	"	74.2

At the end may be seen the graphical representation of the calculated data. In looking at the curves it can be noticed that the efficiency increases gradually up to a certain point, this point being different in each case, as "R" increases. The point at which the abrupt change in the efficiency curve takes place approaches closer to the practical efficiency of pure water as the ratio between the size of sand and size of spigot increases. For example the large spigot, diameter 18.3 m.m., and the large sand, 4 m.m. in diameter, being used the abrupt change in the curve takes place when the efficiency is about 75% and "R" is about 5; while in the case of the small spigot, diameter 6.3 m.m., and the small sand, diameter 0.606 m.m., being used the abrupt change takes place when efficiency is about 80% and "R" is about 4. It was first thought that in plotting the efficiency and "R" the curve would show a gradual increase with no abrupt change, but this did not prove to be the case. In all cases the increase was gradual up to a certain point, then the abrupt change took place.

It is true the nearer we approach pure water the greater the efficiency will be, but this can hardly be used to advantage in practice; however, to use 20 times as much water as sand may be practical and this will give a fairly high efficiency of discharge no matter what size the sand grains may be or what size spigot is used as long as the sand grains are small enough to pass through the spigot without clogging it. A little care must be taken, however, as to the amount of pulp fed to the classifier for most of the pulp must exit through the spigot and it is possible to clog any machine by over feeding it.



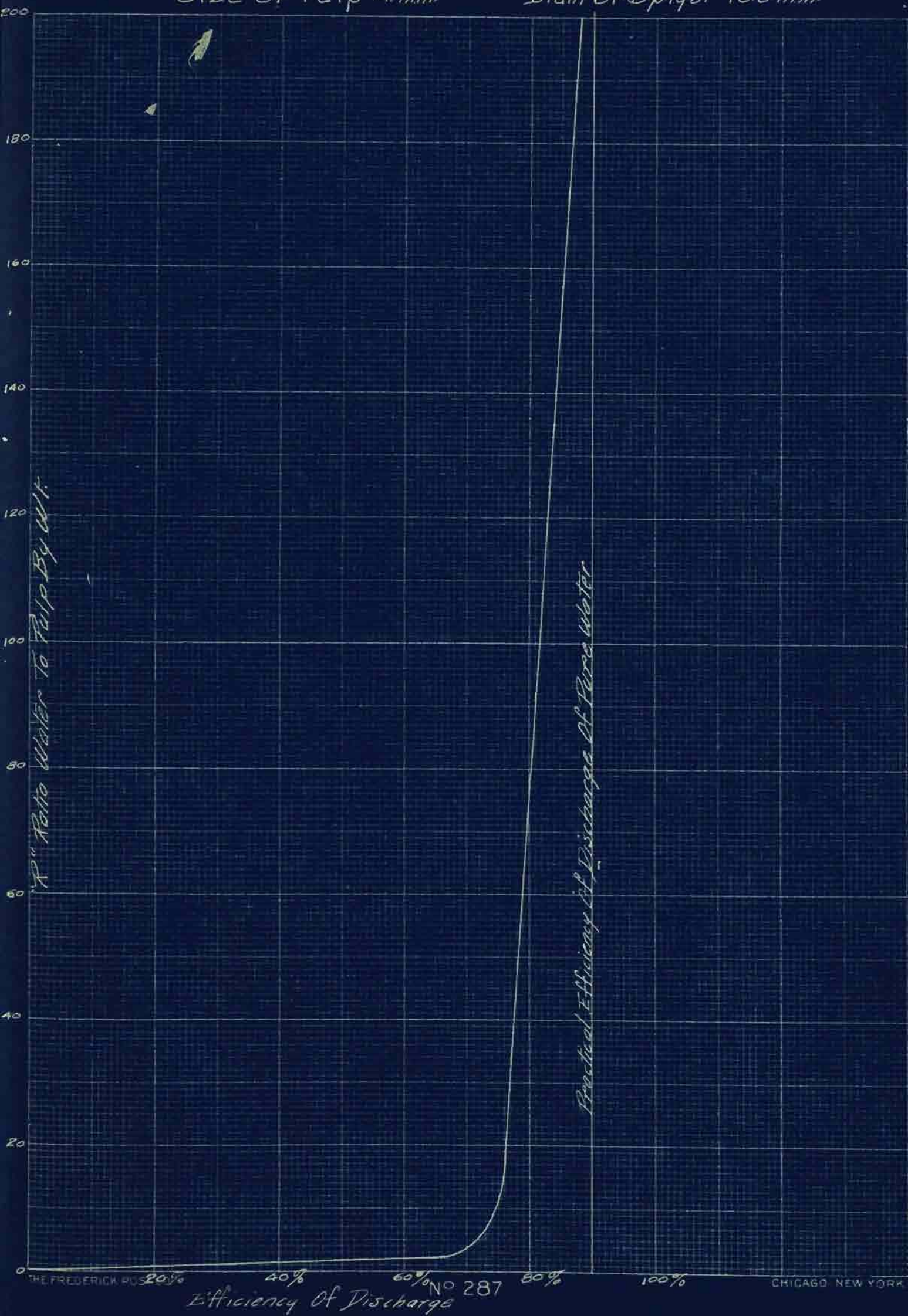
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Size Of Pulp 4 mm.

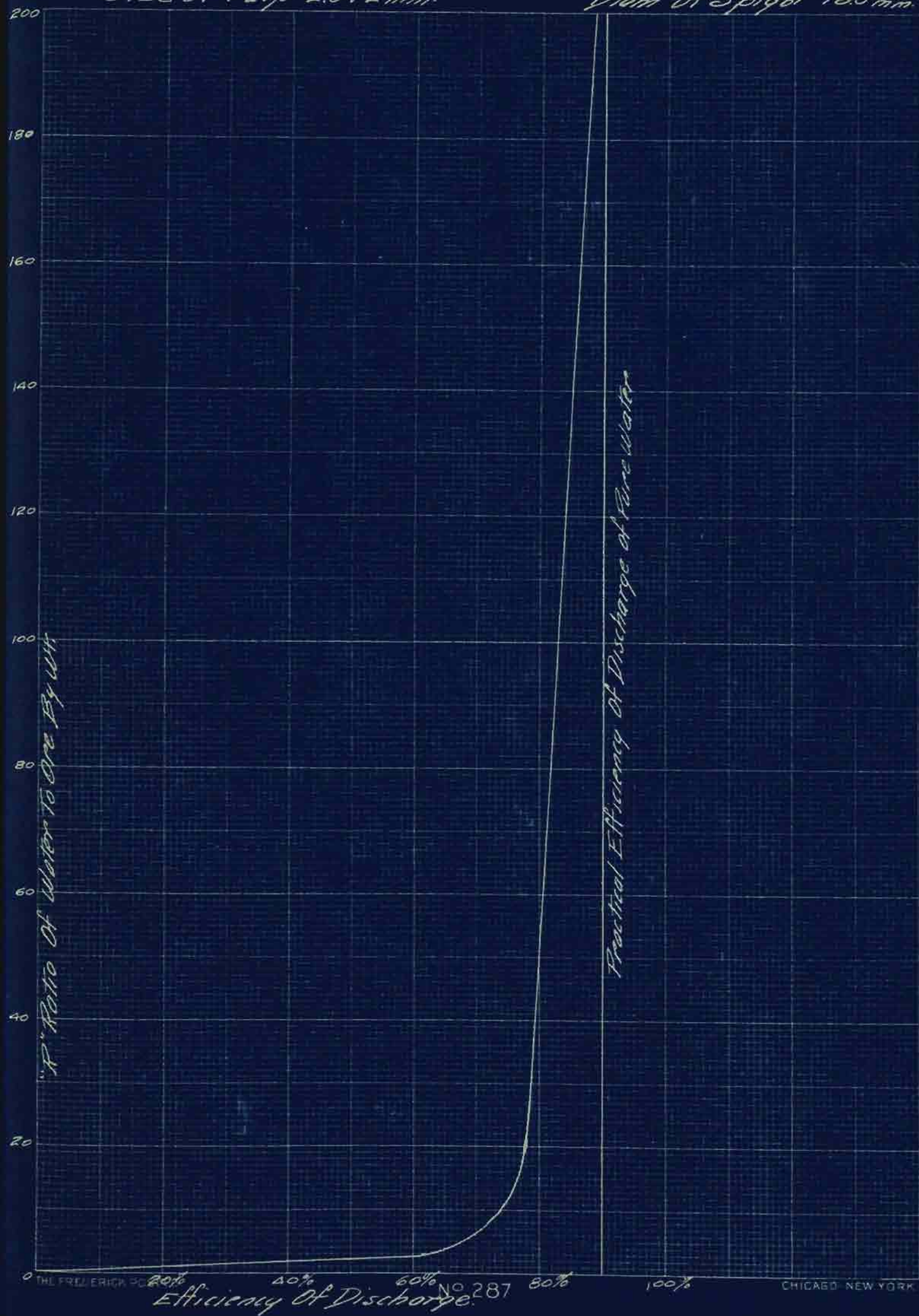
Diam Of Spigot 18.3 mm.





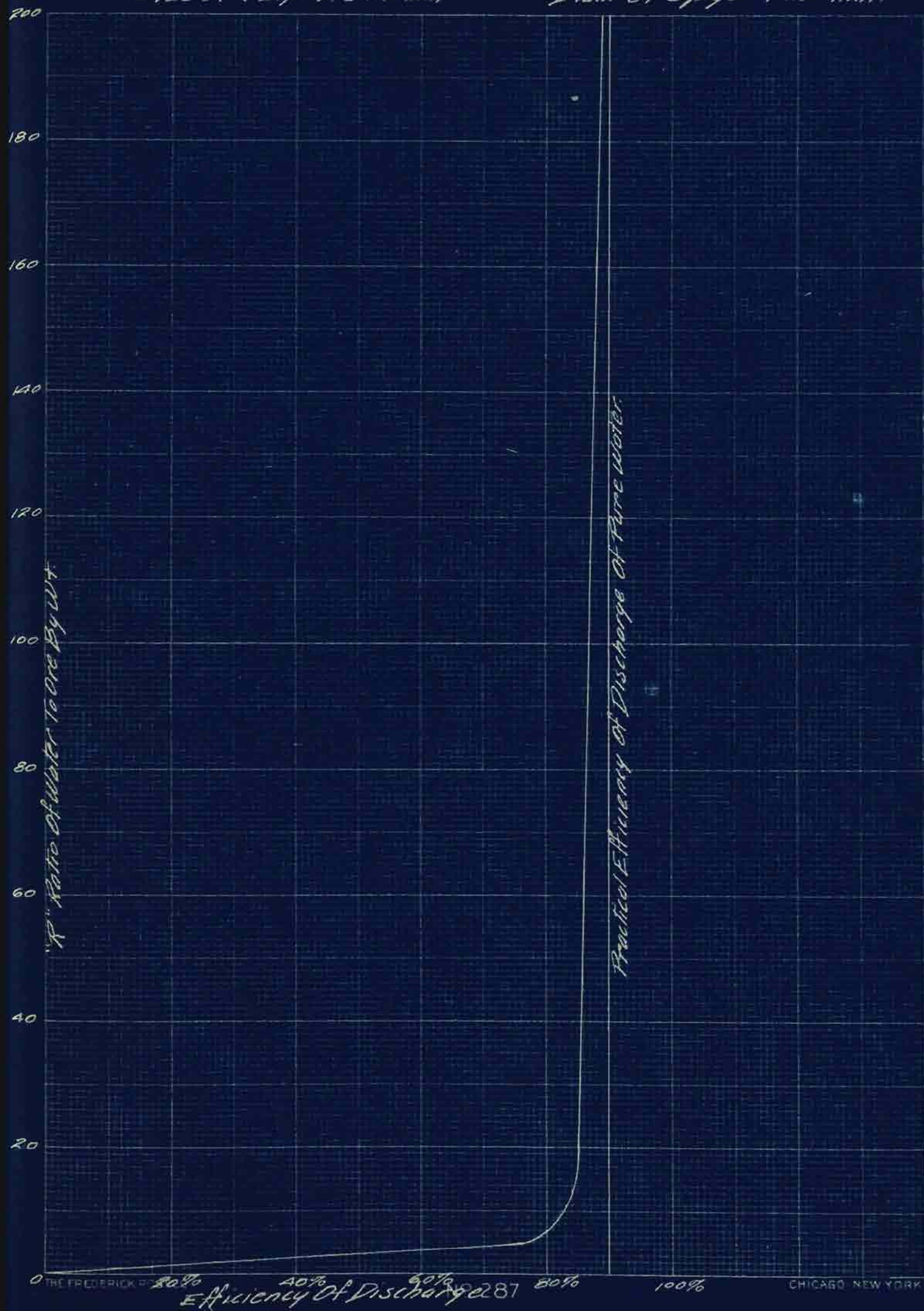
Size Of Pulp 2.972 mm.

Diam Of Spigot 18.3 mm.



Size Of Pulp 2.972 mm

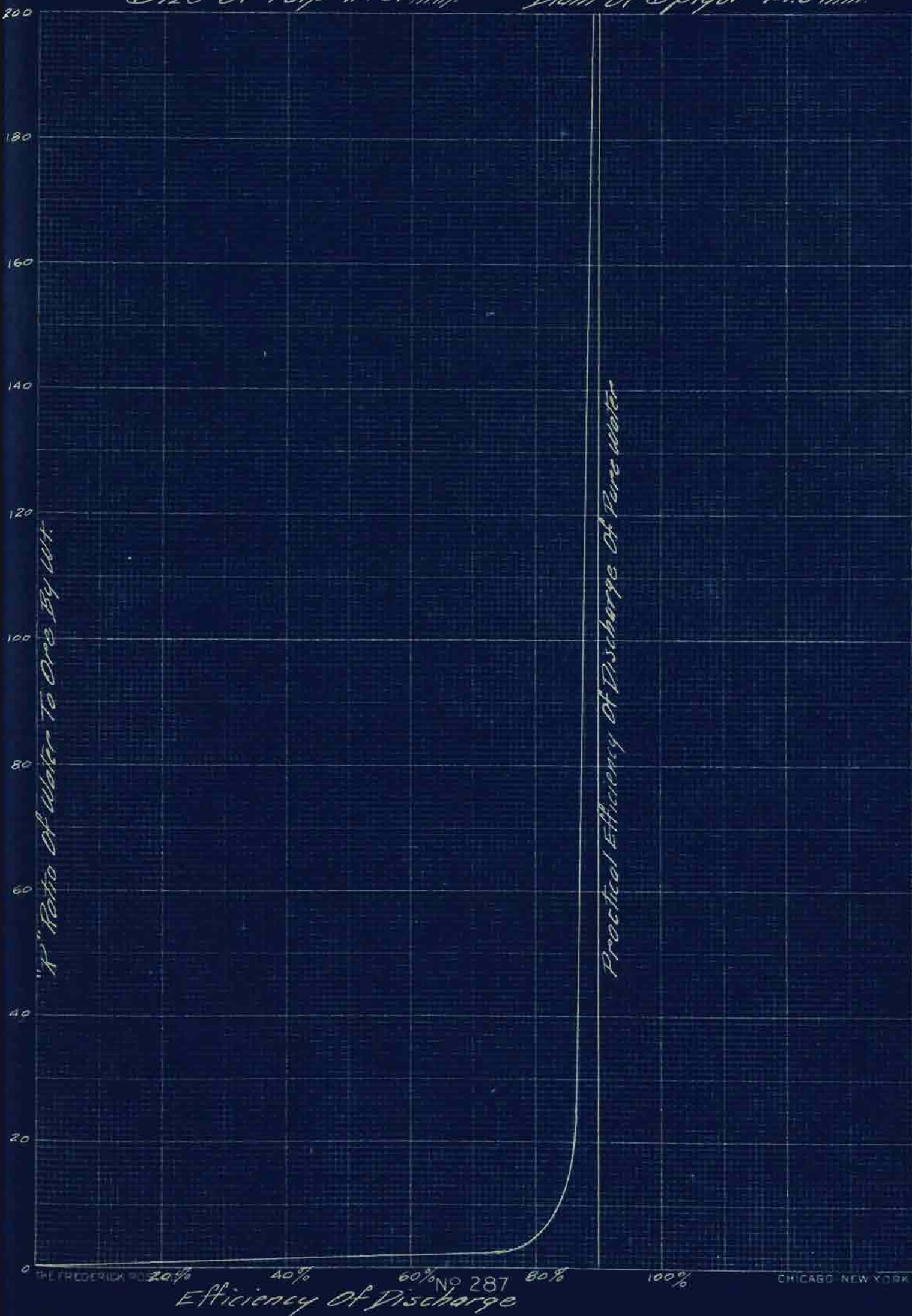
Diam Of Spigot 14.2 mm.





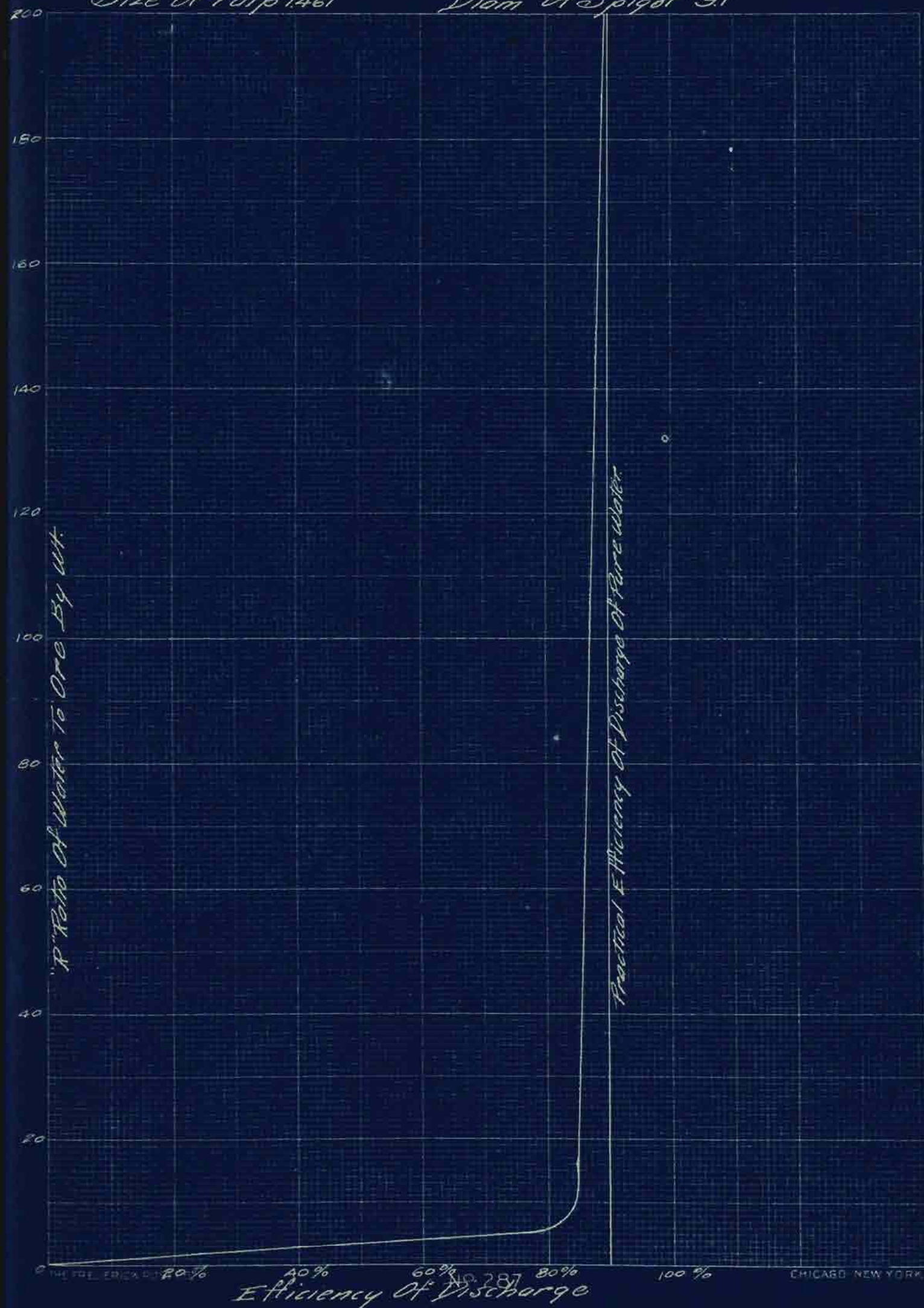
Size Of Pulp 1.461 mm.

Diam Of Spigot 14.3 mm.



Size Of Pulp 1461

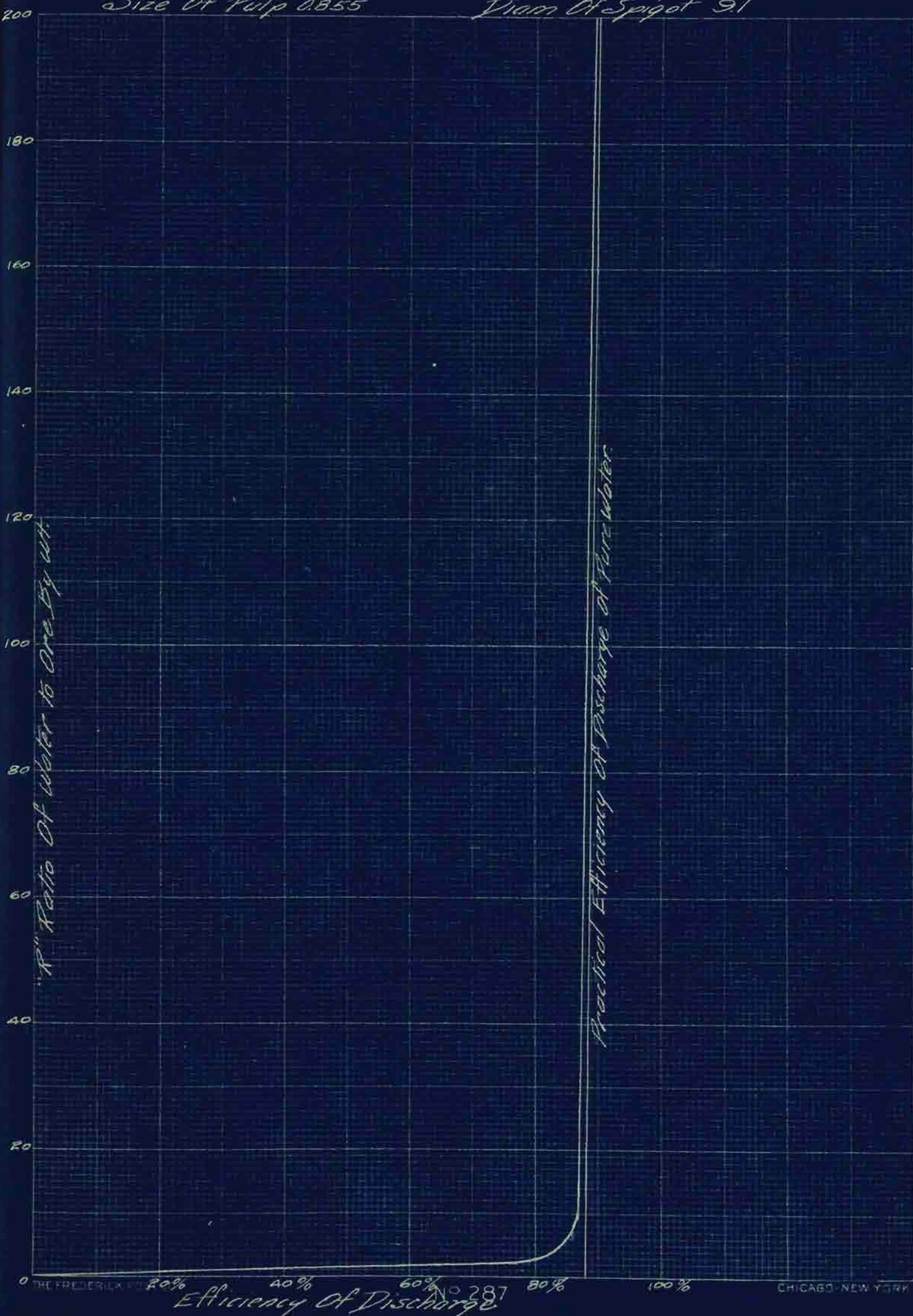
Diam Of Spigot 9.1





Size of Pulp 0855

Diam of Spigot 9.1



Size of Vulp 0.606 mm

Diam of Spigot 9.1 mm.

200

180

160

140

120

100

80

60

40

20

0

20%

40%

60%

80%

100%

CHICAGO NEW YORK

Efficiency of Discharge

"P" Ratio water to one by wt.

Practical Discharge of Pure water

No 287



Size Of Pulp .606 mm

Diam. Of Spigot 6.3 mm.

