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16 Apr 1992

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Kenneth D. Kangas

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### Recommended Citation

Kangas, Kenneth D., "Implementation of T1545 in Air Pressure Control" (1992). Opportunities for Undergraduate Research Experience Program (OURE). 62. [https://scholarsmine.mst.edu/oure/62](https://scholarsmine.mst.edu/oure/62?utm_source=scholarsmine.mst.edu%2Foure%2F62&utm_medium=PDF&utm_campaign=PDFCoverPages) 

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### IMPLEMENTATION OF TI545 IN AIR PRESSURE CONTROL

### Kenneth D. Kangas

### Electrical Engineering Department

### **ABSTRACT**

The Texas Instruments Model 545 programmable logic controller is used to control the air pressure in a heating/ventilation simulator designed and built for a classroom experiment station. Through the use of the PLC's built-in PID algorithm, the pressure in the duct was controlled to within a 2% tolerance and over 72% of the sensor range for a load setting of 10%. The theory of PID controllers and their application to this problem are discussed. Also, the configuration of the simulator, and plans for future work are described.

### **THEORY**

The Proportional-Integral-Derivative (PID) controller, because of its simplicity and effectiveness, is one of the most widely used control schemes in industry. Fundamentally, the PID is a feedback loop with three terms in the feedback transfer function: proportional, integral, and derivative. The proportional term responds to changes in the process variable, but a P controller settles at an offset value that is different from the process set-point. The integral term remedies this problem by responding to the integral of the difference between set-point and process variable values. However, in some circumstances, the integral term can saturate the controller and render it useless. The use of an integral reset coefficient can fix this problem. The derivative term is added in some situations for faster response and better damping characteristics.

### SYSTEM DESCRIPTION

The heating/ventilation simulator (see Figure 1) consists of a piece of ordinary air ducting with a 3-phase blower on one end, a heating element inside, and a variable opening on the other end to simulate varying loads on the H/V system. The blower is driven by an Allen Bradley variable-frequency motor drive, with a range of 0.5 to 60 Hertz. The drive frequency is controlled by a 0-10 Volt analog signal from the PLC. An Omega pressure sensor with a range of  $O-1$   $H<sub>2</sub>O$  is located close to the opening and sends a 4-20 mA analog signal to the PLC.



Figure 1

# **CONTROL**

There are three primary parameters which affect the pressure inside the duct: (1) the speed of the blower, (2) the load setting, and (3) the temperature in the duct. To simplify the investigation, the load was considered to be a system disturbance and not controllable by the PLC. Also, the effect of temperature on the pressure was neglected. In essence, the duct air pressure was considered to be a direct function of only the speed of the blower. The block diagram of this simplified system is shown in Figure 2.



Figure 2

The Laplace transform of the PID loop is given by equation 1.

$$
M = K_c (E + E/(T_i s) + CT_d s) + M_x/s
$$
 (1)

Where:

 $M =$  PID loop output  $E = Set point - process variable$  $C =$  Process variable (pressure in duct)  $M<sub>x</sub>$  = Loop output when  $E = 0$  $K_c$  = Proportional Gain  $T_i$  = Reset coefficient  $T_d$  = Derivative coefficient

As was mentioned before, the PLC has a pre-programmed PID algorithm so that the application engineer has only to "fill in the blanks" to set up and tune the controller. The set-point is held in a special dedicated variable called LSPX (where X is the loop number, 1-64.) In this case, the process variable (C) is contained in WX49, which is the address of the analog pressure sensor value after A-D conversion. The parameters  $K_c$ ,  $T_i$ , and  $T_d$  are directly entered into the PID loop table (Appendix A.) It was found that values of 0.75, 0.09, and 0, respectively, gave the best performance.  $T_{d}$  was set to zero because taking the derivative of the inherently noisy pressure signal puts wild swings into the loop output. This effectively classifies this control as a PI control rather than a PID.

### PERFORMANCE

The PI controller is not aggressively tuned and the settling time equals the rise time. There is no sinusoidal "bouncing" around the set point, so once it is within tolerance, it stays within tolerance. Table 1 shows the 95% rise times when the set point was changed in a step from 10% to another value. For each measurement, the system was allowed to settle at the 10% point before input of the new setpoint value. The control was able to hold the process variable to within 1.3% of the set point. In the table, t, is given in seconds, set-points are given in hundredths of an inch of water (which corresponds to percent of sensor range.)

#### **TABLE 1: RISE TIMES**



# PROGRAMMING

The basic programming tools of the PLC logic are discrete and analog inputs and outputs, control relays, timers, counters, math special functions, and various bit and word manipulation functions. Most of the programming of this project was accomplished in math special functions. The ladder listing and special function listing are in Appendix A.

The basic operation of the system is to use a selector switch  $(X3, X4, X5, X6)$ to choose one of two pressure set-points (or one of two temperature set-points in the future.) Then using momentary push buttons  $(X7-up, X8-down,)$  the set point is incremented up or down by one percent. The value is displayed on an LED readout (Y17-Y24.) When the START button  $(X1)$  is pressed the value from the display is loaded into LSP1 (the PID algorithm's dedicated set-point address,) the loop is set to automatic mode, and the control relay (Y29) for the frequency drive is turned on. The set point may be changed at any time with no effect on the loop until the START button is pressed. Pressing the STOP button (X2) turns off the freq. drive relay and takes the PID loop out of automatic mode. The two lamps (Y26, Y28) are turned on and off by the control loop flag (C106) which shows the sign of the E in the loop. For example, if the system is stepped to 60 from a value of 20, the Error (set-point process variable) will be positive until the process variable becomes greater than the set-point. This was handy for tuning, since one could see the system was settled when the two lights began blinking back and forth rapidly.

# **FUTURE WORK**

Plans for future experimentation consist mainly of developing a temperature control loop, a better user interface, and perhaps implementing a fuzzy controller to replace the PID algorithm. All three of these will be totally software changes, as the temperature control hardware is already in place.

The most immediate of these projects will be the temperature control loop. It will be almost identical in structure to the pressure control loop except that the heating element (driven by a relay) is either off or on. There is no analog control of the heating hardware. Therefore a proportional time control scheme will be implemented, where the output from the PID will go to a math function which will calculate a duty cycle for the heating element. One of the issues to be resolved in this problem will be finding the optimum period of the off/on total cycle.

### **CONCLUSION**

By holding the pressure to within 1 .3 % of the set point, PLC PID controller has proven its viability to an HVAC application. The ease with which the application engineer is able to assemble a working system highlights the flexibility and explains the popularity of the industrial programmable logic controller.

# **ACKNOWLEDGMENTS**

I would like to thank those whose help has made this project possible:

Dr. Kelvin Erickson -- Faculty Advisor

Marvin "Eddie" Light and Donald "Frosty" Foster for building the platform



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**PID LOOP 1 TITLE; PRESSURE POS/VBL PID ALGORITHM: POS LOOP VFLAG ADDRESS: C101 SAMPLE RATE (SECS): +0.10000 PROCESS VARIABLE ADDRESS: WX49 PV RANGE: LOW =**  $+20.0000$ **HIGH \* +100.000 PV IS BIPOLAR: NO SQUARE ROOT OP PV: NO 20% OFFSET ON PV: YES REMOTE SETPOINT: NONE CLAMP SP LIMITS: LOW - +20.0000 HIGH • +100.000 LOOP GAIN: +0.75000 RESET (INTEGRAL TIME): +0.09000 RATE (DERIVATIVE TIME): +0.00000 FREEZE BIAS: NO DERIVATIVE GAIN LIMITING: NO LIMITING COEFFICIENT: +10.0000 SPECIAL CALCULATION ON: NONE SPECIAL FUNCTION: NONE LOOP OUTPUT ADDRESS: WY57 OUTPUT IS BIPOLAR: NO LOCK SETPOINT: NO 20% OFFSET ON OUTPUT: NO LOCK AUTO/MANUAL: NO LOCK CASCADE: NO RAMP/SOAK PROGRAMMED: NO RAMP/SOAK FOR SP: NO ERROR OPERATION: NONE REVERSE ACTING: NO ALARM DEADBAND: +2.00000 MONITOR DEVIATION: NO DEVIATION ALARM: YELLOW \* +3.00000 MONITOR LOW-LOW/HI-HI: NO MONITOR LOW/HIGH: NO PV ALARMS: LOW-LOW \* +41.0000 MONITOR RATE OF CHANGE: NO LOW \* +45.0000 RATE OF CHANGE ALARM: +0.00000**  $HIGH = +55.0000$ **HIGH-HIGH \* +59.0000 MONITOR BROKEN XMITTER: NO**



i.

#### TITLE: SETPT.DN **SF PROGRAM 2**

**CONTINUE ON ERROR (Y,N): NO ERROR STATUS ADDR (Y,C,WY,V): V53 - V55 PROGRAM TYPE (N,P,C,R): PRIORITY CYCLE TIME (SEC): 0.0**



**TITLE: LOOPS.ON SF PROGRAM 3**

**CONTINUE ON ERROR (Y,N): NO ERROR STATUS ADDR (Y,C,WY,V): V56 - V58 PROGRAM TYPE (N,P,C,R): PRIORITY CYCLE TIME (SEC): 0.0**

